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Stack Emissions Testing Report Commissioned by
Furness Brick and Tile Company Ltd

Installation Name & Address
Furness Brick and Tile Company Ltd
Dalton Road
Askam-in-Furness
Cumbria
LA16 7HF

PPC Permit: PPC/A2/01

Stack Reference
Main Kiln Stack

Dates of the Monitoring Campaign
15th - 16th December 2015

Job Reference Number
CEK-1970

Report Written by
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Report Date
30th December 2015

Version
Version 1

Signature of Report Approver


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Executive Summary

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MONITORING OBJECTIVES

Furness Brick and Tile Company Ltd, Askam-in-Furness

Main Kiln Stack

15th - 16th December 2015

Overall Aim of the Monitoring Campaign

Exova Catalyst were commissioned by Furness Brick and Tile Company Ltd to carry out stack emissions testing on the Main Kiln Stack at Askam-in-Furness.

The aim of the monitoring campaign was to demonstrate compliance with a set of emission limit values (ELVs) as specified in the Site's Permit.

Special Requirements

The monitoring campaign for HF was performed over a 24 hour period.

Target Parameters

Total Particulate Matter, Hydrogen Fluoride

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MONITORING RESULTS

Furness Brick and Tile Company Ltd, Askam-in-Furness

Main Kiln Stack

15th - 16th December 2015

where MU = Measurement Uncertainty associated with the Result

Parameter	Concentration				Mass Emission			
	Units	Result	MU +/-	Limit	Units	Result	MU +/-	Limit
Total Particulate Matter	¹ mg/m ³	8.6	0.48	100	g/hr	959	102	-
Hydrogen Fluoride	¹ mg/m ³	1.0	0.07	10	g/hr	113	12.9	-
Water Vapour	% v/v	2.8	0.13					
Stack Gas Temperature	°C	23.0						
Stack Gas Velocity	m/s	7.4	0.58					
Volumetric Flow Rate (ACTUAL)	m ³ /hr	123688	11215					
Volumetric Flow Rate (REF)	¹ m ³ /hr	111904	10146					

NOTE: VOLUMETRIC FLOW RATE DATA TAKEN FROM THE PRELIMINARY VELOCITY TRAVERSE.

¹ Reference Conditions (REF) are: 273K, 101.3kPa, without correction for water vapour content.

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MONITORING DATE(S) & TIMES

Furness Brick and Tile Company Ltd, Askam-in-Furness

Main Kiln Stack

15th - 16th December 2015

Parameter		Units	Concentration	Units	Mass Emission	Sampling Date(s)	Sampling Times	Duration mins
Total Particulate Matter	R1	mg/m ³	4.7	g/hr	522	15/12/2015	11:40 - 14:40	180
Total Particulate Matter	R2	mg/m ³	4.2	g/hr	470	15/12/2015	14:50 - 17:50	180
Total Particulate Matter	R3	mg/m ³	16.8	g/hr	1885	16/12/2015	09:22 - 12:22	180
Hydrogen Fluoride(ISO)	R1	mg/m ³	0.24	g/hr	26.3	15/12/2015	11:40 - 14:40	180
Hydrogen Fluoride(ISO)	R2	mg/m ³	0.48	g/hr	53.9	15/12/2015	14:50 - 17:50	180
Hydrogen Fluoride (non Iso)	R3	mg/m ³	0.69	g/hr	77.6	15/12/2015	18:00 - 00:00	360
Hydrogen Fluoride (non Iso)	R4	mg/m ³	1.3	g/hr	150	16/12/2015	00:10 - 09:10	540
Hydrogen Fluoride(ISO)	R5	mg/m ³	2.3	g/hr	257	16/12/2015	09:22 - 12:22	180
Velocity & Volumetric Flow Rate	R1					15/12/2015	11:25 - 11:40	

All results are expressed at the respective reference conditions.

Executive Summary

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PROCESS DETAILS

Furness Brick and Tile Company Ltd, Askam-in-Furness

Main Kiln Stack

15th - 16th December 2015

Standard Operating Conditions

Parameter	Value
Process Status	Normal
Continuous or Batch Process	Continuous Batch Feed - 5 Week Cycles
Feedstock (if applicable)	Bricks
Abatement System	N/A
Abatement System Running Status	N/A
Fuel	Coal
Plume Appearance	None Visible

Executive Summary

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MONITORING & ANALYTICAL METHODS

Furness Brick and Tile Company Ltd, Askam-in-Furness

Main Kiln Stack

15th - 16th December 2015

Parameter	Monitoring				Analysis				MCERTS Testing	LOD (Average)
	Standard	Technical Procedure	ISO 17025 Testing	Testing Lab	Analytical Procedure	Analytical Technique	ISO 17025 Analysis	Analysis Lab		
Total Particulate Matter	EN 13284-1	CAT-TP-01	Yes	CAT	CAT-TP-03	Gravimetric	Yes	CAT	Yes	0.06 mg/m ³
Hydrogen Fluoride	BS ISO 15713	CAT-TP-10	Yes	CAT	CAT-AP-01	IC	Yes	CAT	Yes	0.013 mg/m ³
Water Vapour	EN 14790	CAT-TP-05	Yes	CAT	CAT-TP-05	Gravimetric	Yes	CAT	Yes	0.1 % v/v
Velocity & Vol. Flow Rate	EN 16911-1 (MID)	CAT-TP-41	Yes	CAT	Pitot Tube and Thermocouple				Yes	1.2 m/s

ANALYSIS LABORATORIES

(with short name reference as appears in the table above)

Exova Catalyst (CAT)	ISO 17025 Accreditation Number: 4279
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SUMMARY OF SAMPLING DEVIATIONS

Parameter	Run	Deviation
Total Particulate Matter	All	Only one sampling line was installed on the stack, however the number of sample points used on the available line were increased to meet the requirements of the Standard.

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SUITABILITY OF SAMPLING LOCATION

Duct Characteristics

Parameter	Units	Value
Type	-	Rectangular
Depth	m	1.57
Width	m	2.97
Area	m ²	4.66
Port Depth	cm	87.0
Orientation of Duct	-	Horizontal
Sample Port Size	-	3" BSP

Location of Sampling Platform

General Platform Information	Value
Permanent / Temporary Platform	Permanent
Inside / Outside	Outside

Platform Details

EA Technical Guidance Note M1 / EN 15259 Platform Requirements	Value
Sufficient working area to manipulate probe and operate the measuring instruments	Yes
Platform has 2 levels of handrails (approx. 0.5m & 1.0m high)	Yes
Platform has vertical base boards (approx. 0.25m high)	Yes
Platform has chains / self closing gates at top of ladders	No
There are no obstructions present which hamper insertion of sampling equipment	Yes
Safe Access Available	Yes
Easy Access Available	Yes

Sampling Location / Platform Improvement Recommendations

In the interest of improved Health and Safety, it would be advantageous to install some form of chain or self closing gate at the top of the sampling platform ladder.

EN 15259 Homogeneity Test Requirements

There is no requirement to perform a EN 15259 Homogeneity Test on this Stack.

Sampling Plane Validation Criteria (from EN 15259)

Criteria in EN 15259	Units	Traverse 1		Required	Compliant
Lowest Differential Pressure	Pa	38.2		> 5 Pa	Yes
Mean Velocity	m/s	7.37		-	-
Lowest Gas Velocity	m/s	6.80		-	-
Highest Gas Velocity	m/s	7.94		-	-
Ratio of Above	: 1	1.17		< 3 : 1	Yes
Maximum Angle of Swirl	°	10.0		< 15°	Yes
No Local Negative Flow	-	Yes		-	Yes

Executive Summary

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PLANT PHOTOS

Photo 1

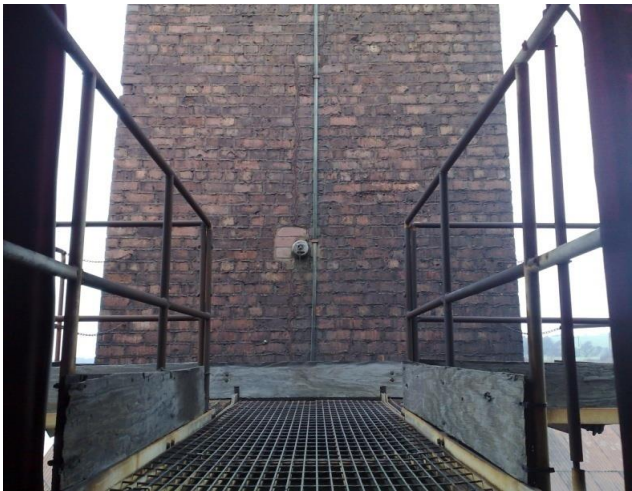
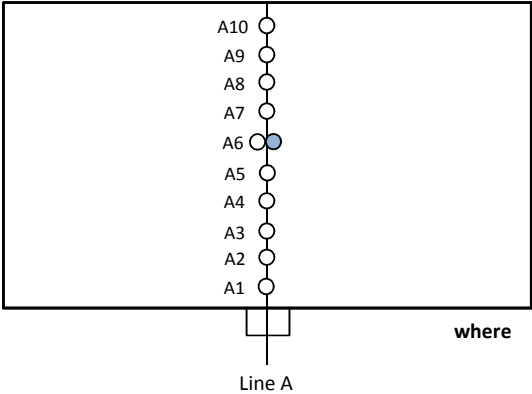


Photo 2



SAMPLE POINTS



- where

○ = isokinetic point sampled at

● = isokinetic point not sampled at

● = combustion gases sample point

● = non-isokinetic sample point

APPENDIX CONTENTS

APPENDIX 1 - Stack Emissions Monitoring Personnel, List of Equipment & Methods and Technical Procedures Used

APPENDIX 2 - Summaries, Calculations, Raw Data and Charts

STACK EMISSIONS MONITORING PERSONNEL

Position	Name	MCERTS Accreditation	MCERTS Number	Technical Endorsements
Team Leader	Stephen Dick	MCERTS Level 2	MM 10 1061	TE1 TE2 TE3 TE4
Technician	Graham Grant	MCERTS Level 1	MM 11 1142	None

LIST OF EQUIPMENT

Extractive Sampling		Instrumental Analysers		Miscellaneous Items	
Equipment Type	Equipment I.D.	Equipment Type	Equipment I.D.	Equipment Type	Equipment I.D.
Control Box DGM (1)	CAT 7.38	Horiba PG-250	CAT 9.10	Digital Manometer (1)	CAT 3.54
Control Box DGM (2)	-	Horiba PG-250 SRM	-	Digital Manometer (2)	CAT 3.54
Box Thermocouples (1)	CAT 3.57	Servomex 4900	-	Digital Temperature Meter	CAT 3.54
Box Thermocouples (2)	-	Eco Physics CLD 822Mh	-	Stopwatch	CAT 14.4 / 14.53
Umbilical (1)	CAT 3.57	ABB AO2020-URAS26	-	Barometer	CAT 13.24
Umbilical (2)	-	Servomex 5200MP	-	Stack Thermocouple (1)	CAT 4.240
Oven Box (1)	CAT 12.963	JCT JCC P1 Cooler	CAT 4.206	Stack Thermocouple (2)	CAT 4.573
Oven Box (2)	-	Gasmet DX4000	-	Stack Thermocouple (3)	CAT 4.585 / 4.702
Heated Probe (1)	CAT 5.4	Gasmet Sampling System	-	1m Heated Line (1)	-
Heated Probe (2)	CAT 5.8	Bernath 3006 FID	-	1m Heated Line (2)	-
Heated Probe (3)	CAT 5.11	Ankersmid APP100	CAT 12.72	1m Heated Line (3)	-
S-Pitot (1)	CAT 21S.4 / 21S.28	Mass Flow Controller (1)	CAT 6.11	5m Heated Line (1)	CAT 20.4
S-Pitot (2)	CAT 21S.26 / 21P.33	Mass Flow Controller (2)	CAT 6.12	15m Heated Line (1)	-
L-Pitot	CAT 21L.4	Mass View (1)	CAT 25.3	20m Heated Line (1)	CAT 20.8
500g Check Weight	CAT 17.4	Mass View (2)	CAT 25.4	20m Heated Line (2)	-
1Kg Check Weight	CAT 17.4	Easylogger EN-EL-12 Bit	CAT 11.19	Dual Channel Heater Controller	CAT 3.15
Last Impinger Arm	CAT 4.22 / 4.24 / 4.99	Easylogger EN-EL-12 Bit	CAT 11.6	Single Channel Heater Controller	-
Callipers	CAT 23.22	Bioaerosols Temperature Logger	-	Laboratory Balance	CAT 1.18 / 1.18a
Tubes Kit Thermocouple	CAT 4.217	Electronic Refrigerator	-	Tape Measure	CAT 16.3

METHODS & TECHNICAL PROCEDURES USED

Parameter	Standard	Technical Procedure
Total Particulate Matter	EN 13284-1	CAT-TP-01
Hydrogen Fluoride	BS ISO 15713	CAT-TP-10
Water Vapour	EN 14790	CAT-TP-05
Velocity & Vol. Flow Rate	EN 16911-1 (MID)	CAT-TP-41

PRELIMINARY STACK SURVEY: CALCULATIONS

General Stack Details

Stack Details (from Traverse)	Units	Value
Stack Diameter / Depth, D	m	1.57
Stack Width, W	m	2.97
Stack Area, A	m ²	4.66
Average Stack Gas Temperature, T _a	°C	23.0
Average Stack Gas Pressure	mmH ₂ O	4.6
Average Stack Static Pressure, P _{static}	kPa	0.077
Average Barometric Pressure, P _b	kPa	99.3
Average Pitot Tube Calibration Coefficient, C _p	-	0.84

Stack Gas Composition & Molecular Weights

Component	Conc ppm	Conc Dry % v/v	Conc Wet % v/v	Volume Fraction r	Molar Mass M	Density kg/m ³ p	Conc kg/m ³ p _i
CO ₂ (Estimated)	-	0.06	0.06	0.0006	44.01	1.9635	0.00118
O ₂ (Estimated)	-	20.80	20.21	0.2080	32.00	1.4277	0.29696
N ₂	-	79.14	76.89	0.7914	28.01	1.2498	0.98913
Moisture (H ₂ O)	-	-	2.85	0.0285	18.02	0.8037	0.02289

Where: $p = M / 22.41$

$p_i = r \times p$

Calculation of Stack Gas Densities

Determinand	Units	Result
Dry Density (STP), P _{STD}	kg/m ³	1.287
Wet Density (STP), P _{STW}	kg/m ³	1.273
Dry Density (Actual), P _{Actual}	kg/m ³	1.165
Average Wet Density (Actual), P _{ActualW}	kg/m ³	1.152

Where: P_{STD} = sum of component concentrations, kg/m³ (not including water vapour)

P_{STW} = sum of all wet concentrations / 100 x density, kg/m³ (including water vapour)

$P_{Actual} = P_{STD} \times (T_{STP} / (P_{STP})) \times ((P_{static} + P_b) / T_a)$

$P_{ActualW}$ (at each sampling point) = P_{STW} x (T_s / P_s) x (P_a / T_a)

Calculation of Stack Gas Volumetric Flowrate, Q

Duct gas flow conditions	Units	Actual	REF ¹
Temperature	°C	23.0	0.0
Total Pressure	kPa	99.4	101.3
Moisture	%	2.85	2.85

Gas Volumetric Flowrate (from Traverse)	Units	Result
Gas Volumetric Flowrate (Actual)	m ³ /hr	123688
Gas Volumetric Flowrate (STP, Wet)	m ³ /hr	111904
Gas Volumetric Flowrate (STP, Dry)	m ³ /hr	108718
Gas Volumetric Flowrate REF ¹	m ³ /hr	111904

PRELIMINARY STACK SURVEY: VELOCITY TRAVERSE TO EN 16911-1 (MID)

(1 of 1)

Parameter	Units	Value
Date of Survey	-	15/12/2015
Time of Survey	-	11:25 - 11:40
Atmospheric Pressure	kPa	99.3
Average Stack Static Pressure	Pa	77
Result of Pitot Stagnation Test	-	Pass
Are Water Droplets Present?	-	No
Device Used	S-Type Pitot with KIMO MP 200 (500Pa)	

Parameter	Units	Value
Initial Pitot Leak Check	-	Pass
Final Pitot Leak Check	-	Pass
Orientation of Duct	-	Horizontal
Pitot Tube, C_p	-	0.84
Number of Lines Available	-	1
Number of Lines Used	-	1

Sampling Line A						
Traverse Point	Depth m	ΔP mmH ₂ O	Temp °C	Wet Density kg/m ³	Velocity m/s	Swirl °
STATIC (Units: Pa)		77.0				
Mean		4.6	23.0	1.152	7.37	
1	0.08	3.9	22.8	1.153	6.80	5.0
2	0.24	4.2	22.9	1.153	7.06	6.0
3	0.39	4.4	23.0	1.152	7.23	7.0
4	0.55	4.6	23.0	1.152	7.39	9.0
5	0.71	5.1	23.0	1.152	7.78	8.0
6	0.86	4.5	23.1	1.152	7.31	7.0
7	1.02	4.2	23.1	1.152	7.06	9.0
8	1.18	5.3	23.1	1.152	7.94	10.0
9	1.33	4.7	23.1	1.152	7.47	9.0
10	1.49	4.9	23.1	1.152	7.63	8.0

PRELIMINARY STACK SURVEY: VELOCITY TRAVERSE TO EN 16911-1 (MID) - MEASUREMENT UNCERTAINTY

(1 of 1)

Performance characteristics (Uncertainty Components)	Uncertainty	Value	Units
Standard Uncertainty on the coefficient of the Pitot Tube	$u(k)$	0.005	-
Standard Uncertainty associated with the mean local dynamic pressures	$u(\Delta p_i)$	1.149	Pa
- Resolution	$u(res)$	0.00087	
- Calibration	$u(cal)$	0.210	
- Drift	$u(drift)$	0.083	
- Lack of Fit	$u(fit)$	0.025	
- Overall corrections to dynamic measurements	$u(C_f)$	0.320	
Standard uncertainty associated with the molar mass of the gas	$u(M)$	0.00003	-
- $\phi O_{2,w}$	-	20.208	
- $\phi CO_{2,w}$	-	0.058	
- Oxygen, dry	$u(\phi O_{2,d})$	0.637	
- Carbon Dioxide, dry	$u(\phi CO_{2,d})$	0.002	
- Water Vapour	$u(\phi H_2O)$	0.145	
- Oxygen, wet	$u(\phi O_{2,w})$	0.619	
- Carbon Dioxide, wet	$u(\phi CO_{2,w})$	0.002	
Standard uncertainty associated with the stack temperature	$u(T_c)$	1.510	K
Standard uncertainty associated with the absolute pressure in the duct	$u(p_c)$	175.696	Pa
- Atmospheric Pressure	$u(p_{atm})$	175.692	
- Static Pressure	$u(p_{stat})$	1.149	
Standard uncertainty associated with the density in the duct	$u(\rho)$	0.00622	-
Standard uncertainty associated with the local velocities	$u(v_i)$	0.928	Pa
Standard uncertainty associated with the mean velocity	$u(\bar{v})$	0.295	m/s
Standard uncertainty associated with the mean velocity (95% Confidence)	$U_c(v)$	0.579	m/s
Standard uncertainty associated with the mean velocity (95% Confidence), relative	$U_{c,rel}(v)$	7.86	%
Standard uncertainty associated with the volume flow rate (95% Confidence)	$U_c(qV,w)$	11214.5	m ³ /hr
- $u^2(a)/a^2$	-	0.00053	
- $u^2(qV,w)/q^2V,w$	-	0.00214	
- $u^2(qV,w)$	-	32737673	
- $u(qV,w)$	-	5721.7	
Standard uncertainty associated with the volume flow rate (95% Confidence), relative	$U_{c,rel}(qV,w)$	9.07	%

TOTAL PARTICULATE MATTER: RESULTS SUMMARY

Furness Brick and Tile Company Ltd, Askam-in-Furness
Main Kiln Stack

Sample Runs

Parameter	Units	Run 1	Run 2	Run 3		Mean
Concentration	mg/m ³	4.7	4.2	16.8		8.6
Uncertainty	±mg/m ³	0.29	0.28	0.86		0.48
Mass Emission	g/hr	522	470	1885		959
Uncertainty	±g/hr	57.6	53.0	196		102

Parameter	Units	Run 1	Run 2	Run 3		Mean
Water Vapour	% v/v	3.0	3.1	2.5		2.9
Uncertainty	±% v/v	0.15	0.16	0.13		0.14

NOTE: Where water droplets are present (See the Quality Assurance page), the Water Vapour concentration as found in Annex A of EN 14790 has been reported instead of the calculated value.

Blank Runs

Parameter	Units	Blank 1	Blank 2		Maximum
Concentration	mg/m ³	0.14	0.13		0.14

General Sampling Information

Parameter	Value	
Standard	EN 13284-1	
Technical Procedure	CAT-TP-01	
Probe Material	Monel	
Filter Housing Material	Monel	
Positioning of Filter	In Stack	
Filter Size and Material	47mm Quartz Fibre	
Number of Sampling Lines Used	1 / 3	FORMAT: Number Used / Number Required
Number of Sampling Points Used	10 / 10	FORMAT: Number Used / Number Required
Sample Point I.D.'s	A1, A2, A3, A4, A5, A6, A7, A8, A9 & A10.	

Reference Conditions

Reference Conditions are: 273K, 101.3kPa, without correction for water vapour content.

TOTAL PARTICULATE MATTER: ISOKINETIC SAMPLING CALCULATIONS

Test	Units	Run 1	Run 2	Run 3	
Absolute pressure of stack gas, P_s					
Barometric pressure, P_b	mmHg	744.8	744.8	744.8	
Stack static pressure, P_{static}	mmH ₂ O	7.9	7.9	7.9	
$P_s = (P_b + (P_{static} / 13.6))$	mmHg	745.3	745.3	745.3	
Volume of water vapour collected, V_{wstd}					
Total mass collected in impingers (liquid trap)	g	25.5	46.5	38.1	
Total mass collected in impingers (silica trap)	g	37.8	17.0	3.3	
Total mass of liquid collected, V_{lc}	g	63.3	63.5	41.4	
$V_{wstd} = (0.001246)(V_{lc})$	m ³	0.0789	0.0791	0.0516	
Volume of gas metered dry, V_{mstd}					
Volume of gas sample through gas meter, V_m	m ³	2.3479	2.2656	2.0479	
Gas meter correction factor, Y_d	-	1.0580	1.0580	1.0580	
Average dry gas meter temperature, T_m	°C	20.6	23.0	18.6	
Average pressure drop across orifice, ΔH	mmH ₂ O	19.7	18.6	15.7	
$V_{mstd} = ((0.3592)(V_m)(P_b + (\Delta H/13.6))(Y_d)) / (T_m + 273)$	m ³	2.2681	2.1703	1.9906	
Moisture content, B_{wo} & R_{ww}					
$B_{wo} = V_{wstd} / (V_{mstd} + V_{wstd})$	m ³	0.0336	0.0352	0.0253	
B_{wo} as a percentage	% v/v	3.36	3.52	2.53	
Reported Water Vapour, checked with Tables in EN 14790, R_{ww}	% v/v	2.96	3.14	2.53	
Volume of gas metered wet, V_{mstw}					
$V_{mstw} = (V_{mstd})(100/(100 - R_{ww}))$	m ³	2.3373	2.2407	2.0421	
Volume of gas metered at Oxygen Reference Conditions, $V_{mstd@X\%O_2}$ & $V_{mstw@X\%O_2}$					
IED & Incinerates Hazardous Material? (Yes = no positive O ₂ correction)	-	No	No	No	
% wet oxygen measured in gas stream, ACT%O _{2w}	% v/v	N/A	N/A	N/A	
% dry oxygen measured in gas stream, ACT%O _{2d}	% v/v	N/A	N/A	N/A	
% oxygen reference condition, REF%O ₂	% v/v	N/A	N/A	N/A	
O ₂ Reference Factor wet ($O_{2REFw} = (21 - REF\%O_2) / (21 - ACT\%O_{2w})$)	-	N/A	N/A	N/A	
O ₂ Reference Factor dry ($O_{2REFd} = (21 - REF\%O_2) / (21 - ACT\%O_{2d})$)	-	N/A	N/A	N/A	
$V_{mstw@X\%oxygen} = (V_{mstw}) / (O_{2REFw})$	m ³	N/A	N/A	N/A	
$V_{mstd@X\%oxygen} = (V_{mstd}) / (O_{2REFd})$	m ³	N/A	N/A	N/A	
Molecular weight of dry gas stream, M_d					
CO ₂ (Estimated)	% v/v	0.06	0.06	0.06	
O ₂ (Estimated)	% v/v	20.80	20.80	20.80	
Total	% v/v	20.86	20.86	20.86	
N ₂	% v/v	79.14	79.14	79.14	
$M_d = 0.44(\%CO_2) + 0.32(\%O_2) + 0.28(\%N_2)$	g/gmol	28.84	28.84	28.84	
Molecular weight of stack gas (wet), M_s					
$M_s = M_d(1 - (R_{ww}/100)) + 18(R_{ww}/100)$	g/gmol	28.52	28.50	28.57	
Velocity of stack gas, V_s					
Pitot tube velocity constant, K_p	-	34.97	34.97	34.97	
Velocity pressure coefficient, C_p	-	0.85	0.85	0.85	
Average of velocity heads, ΔP_{avg}	mmH ₂ O	5.30	4.88	4.23	
Average square root of velocity heads, $\sqrt{\Delta P}$	√mmH ₂ O	2.30	2.21	2.06	
Average stack gas temperature, T_s	°C	23.5	24.8	28.0	
$V_s = ((K_p)(C_p)(\sqrt{\Delta P})(V_{Ts} + 273)) / (V(M_s)(P_s))$	m/s	8.10	7.79	7.28	
Total flow of stack gas: Actual (Q_a), Wet (Q_{stw}), Dry (Q_{std}), Wet@O_{2REF} (Q_{stwO_2}), Dry@O_{2REF} (Q_{stdO_2})					
Area of stack, A_s	m ²	4.66	4.66	4.66	
$Q_a = (60)(A_s)(V_s)$	m ³ /min	2266.0	2180.5	2037.2	
Conversion factor (K/mm.Hg), C_f	-	0.3592	0.3592	0.3592	
$Q_{stw} = ((Q_a)(P_s)(C_f)) / ((T_s) + 273)$	m ³ /min	2045.9	1960.3	1811.9	
$Q_{std} = ((Q_a)(P_s)(C_f)(1 - (R_{ww}/100))) / ((T_s) + 273)$	m ³ /min	1985.3	1898.8	1766.1	
$Q_{stwO_2} = ((Q_a)(P_s)(C_f)) / ((T_s) + 273) / (O_{2REFw})$	m ³ /min	N/A	N/A	N/A	
$Q_{stdO_2} = ((Q_a)(P_s)(C_f)(1 - (R_{ww}/100))) / ((T_s) + 273) / (O_{2REFd})$	m ³ /min	N/A	N/A	N/A	
Percent isokinetic, %I					
Nozzle diameter, D_n	mm	6.05	6.05	6.05	
Nozzle area, A_n	mm ²	28.72	28.72	28.72	
Total sampling time, q	min	180	180	180	
$\%I = (4.6398E^6)(T_s + 273)(V_{mstd}) / (P_s)(V_s)(A_n)(q)(1 - (R_{ww}/100))$	%	103.0	103.1	101.7	

TOTAL PARTICULATE MATTER: SAMPLING DETAILS

Sample Runs

Parameter	Units	Run 1	Run 2	Run 3	
Sampling Times	-	11:40 - 14:40	14:50 - 17:50	09:22 - 12:22	
Sampling Dates	-	15/12/2015	15/12/2015	16/12/2015	
Sampling Device	-	ISO	ISO	ISO	
Volume Sampled (REF)	m ³	2.3373	2.2407	2.0421	
Filter I.D. Number	-	90-4656	47-28632	47-29669	
Start Filter Mass	g	0.52571	0.13786	0.14700	
End Filter Mass	g	0.53017	0.14149	0.14887	
Total Mass on Filter	g	0.00446	0.00363	0.00187	
Probe Rinse I.D. Number	-	PR-90-4656	PR-47-28632	PR-47-29669	
Start Probe Rinse Mass	g	2.99616	3.06594	3.07137	
End Probe Rinse Mass	g	3.00260	3.07173	3.10389	
Total Mass in Probe Rinse	g	0.00644	0.00579	0.03252	
Total Mass Collected	mg	10.90	9.42	34.39	
Calculated Concentration	mg/m ³	4.66	4.20	16.84	
Balance Uncertainty / LOD	mg/m ³	0.06	0.06	0.06	

Where: ISO stands for Manual Isokinetic Sampling Train

Blank Runs

Parameter	Units	Blank 1	Blank 2	
Blank Dates	-	15/12/2015	16/12/2015	
Average Volume Sampled (REF)	m ³	2.2067	2.2067	
Filter I.D. Number	-	47-30204	47-29692	
Start Filter Mass	g	0.14856	0.14533	
End Filter Mass	g	0.14861	0.14541	
Total Mass on Filter	g	0.00005	0.00008	
Probe Rinse I.D. Number	-	PR-47-30204	PR-47-29692	
Start Probe Rinse Mass	g	3.08844	3.04260	
End Probe Rinse Mass	g	3.08869	3.04280	
Total Mass in Probe Rinse	g	0.00025	0.00020	
Total Mass Collected	mg	0.30	0.28	
Calculated Concentration	mg/m ³	0.14	0.13	
Balance Uncertainty / LOD	mg/m ³	0.06	0.06	

TOTAL PARTICULATE MATTER: QUALITY ASSURANCE

(PAGE 1 OF 2)

Sample Runs

Leak Test Results	Units	Run 1	Run 2	Run 3	
Mean Sampling Rate	l/min	13.80	13.32	12.04	
Pre-Sampling Leak Rate	l/min	0.06	0.15	0.09	
Post-Sampling Leak Rate	l/min	0.14	0.11	0.14	
Allowable Leak Rate	l/min	0.28	0.27	0.24	
Leak Test Acceptable	-	Yes	Yes	Yes	
Water Droplets	Units	Run 1	Run 2	Run 3	
Are Water Droplets Present	-	Yes	Yes	No	
MU (Concurrent Water Vapour)	Units	Run 1	Run 2	Run 3	
Measurement Uncertainty (MU)	%	5.0	5.0	5.1	
Allowable MU	%	20	20	20	
MU Acceptable	%	Yes	Yes	Yes	
Silica Gel (Concurrent Water Vapour)	Units	Run 1	Run 2	Run 3	
Less than 50% Faded	%	Yes	Yes	Yes	
Isokinetic Criterion Compliance	Units	Run 1	Run 2	Run 3	
Isokinetic Variation	%	103.0	103.1	101.7	
Allowable Isokinetic Range	%	95 - 115	95 - 115	95 - 115	
Isokineticity Acceptable	-	Yes	Yes	Yes	
Weighing Uncertainty Criteria	Units	Run 1	Run 2	Run 3	
Overall Weighing Uncertainty	± mg	0.24	0.24	0.24	
Overall Weighing Uncertainty	± mg/m ³	0.10	0.11	0.12	
ELV [Daily ELV for IED]	mg/m ³	100.00	100.00	100.00	
Allowable Weighing Uncertainty	mg/m ³	5.00	5.00	5.00	
Weighing Uncertainty Acceptable	-	Yes	Yes	Yes	
Filter Temperatures	Units	Run 1	Run 2	Run 3	
Pre-Conditioning Temperature	°C	180	180	180	
Post-Conditioning Temperature	°C	160	160	160	
Maximum Filter Temperature	°C	24	25	28	
Test Conditions	Units	Run 1	Run 2	Run 3	
Ambient Temperature Recorded?	-	Yes	Yes	Yes	

TOTAL PARTICULATE MATTER: QUALITY ASSURANCE

(PAGE 2 OF 2)

Blank Runs

Leak Test Results	Units	Blank 1	Blank 2	
Expected Sampling Rate	l/min	15.00	15.00	
Pre-Sampling Leak Rate	l/min	0.09	0.11	
Post-Sampling Leak Rate	l/min	0.13	0.15	
Allowable Leak Rate	l/min	0.30	0.30	
Leak Test Acceptable	-	Yes	Yes	

Validity of Blank vs ELV	Units	Blank 1	Blank 2	
Allowable Blank	mg/m ³	10.0	10.0	
Blank Acceptable	-	Yes	Yes	

Acetone / Water Rinse Blank	Units	Blank
Acetone / Water Rinse Value	mg/l	2.7
Allowable Blank	mg/l	10
Blank Acceptable	-	Yes

Method Deviations

Nature of Deviation	Run Number			
	1	2	3	
(x = deviation applies to the associated run, wx = deviation also applies to the concurrent water vapour run)				
Only one sampling line was installed on the stack, however the number of sample points used on the available line were increased to meet the requirements of the Standard.	x	x	x	

TOTAL PARTICULATE MATTER: MEASUREMENT UNCERTAINTY CALCULATIONS

Measured Quantities	Value					Standard uncertainty					
	Symbol	Run 1	Run 2	Run 3		Symbol	Units	Run 1	Run 2	Run 3	
Sampled Volume (Actual)	V _m	2.3479	2.2656	2.0479		uV _m	m ³	0.0470	0.0453	0.0410	
Sampled Gas Temperature	T _m	293.6	296.0	291.6		uT _m	K	2.0	2.0	2.0	
Sampled Gas Pressure	p _m	99.4	99.4	99.4		up _m	kPa	0.5	0.5	0.5	
Sampled Gas Humidity	H _m	0.0	0.0	0.0		uH _m	% v/v	1.0	1.0	1.0	
Leak	L	1.01	0.83	1.16		uL	%	-	-	-	
Mass of Particulate	m	10.90	9.42	34.39		um	mg	0.13	0.13	0.13	
Uncollected Mass	UCM	0.30	0.30	0.30		uUCM	mg	-	-	-	

Measured Quantities	Uncertainty as a Percentage					Requirement of Standard
	Units	Run 1	Run 2	Run 3		
Sampled Volume (Actual)	%	2.00	2.00	2.00		≤2%
Sampled Gas Temperature	%	0.68	0.68	0.69		≤1%
Sampled Gas Pressure	%	0.50	0.50	0.50		≤1%
Sampled Gas Humidity	%	1.00	1.00	1.00		≤1%
Leak	%	1.01	0.83	1.16		≤2%
Mass of Particulate	%	0.06	0.06	0.06		<5% of ELV
Uncollected Mass	%	-	-	-		-

Measured Quantities	Uncertainty in Measurement Units						Sensitivity Coefficient			
	Symbol	Units	Run 1	Run 2	Run 3		Run 1	Run 2	Run 3	
Sampled Volume (STP)	V _m	m ³	2.2681	2.1703	1.9906		2.06	1.94	8.46	
Leak	L	mg/m ³	0.027	0.020	0.113		1.00	1.00	1.00	
Mass of Particulate	L _r	mg	10.900	9.420	34.393		0.43	0.45	0.49	
Uncollected Mass	UCM	mg	0.17	0.17	0.17		0.43	0.45	0.49	

Measured Quantities	Uncertainty in Result				
	Units	Run 1	Run 2	Run 3	
Sampled Volume (STP)	mg/m ³	0.114	0.104	0.411	
Leak	mg/m ³	0.0273	0.0200	0.1131	
Mass of Particulate	mg/m ³	0.0556	0.0580	0.0637	
Uncollected Mass	mg/m ³	0.0741	0.0773	0.0848	

Measured Quantities	Oxygen Correction Part of MU Budget				
	Units	Run 1	Run 2	Run 3	
O ₂ Correction Factor	-	N/A	N/A	N/A	
Stack Gas O ₂ Content	% v/v	N/A	N/A	N/A	
MU for O ₂ Correction	-	N/A	N/A	N/A	
Overall MU For O ₂ Measurement	%	N/A	N/A	N/A	

Parameter	Units	Run 1	Run 2	Run 3	
Combined uncertainty	mg/m ³	0.15	0.14	0.44	
Expanded uncertainty (95% confidence), without Oxygen Correction	mg/m ³	0.29	0.28	0.86	
Expanded uncertainty (95% confidence), with Oxygen Correction	mg/m ³	N/A	N/A	N/A	
Expanded uncertainty (95% confidence), estimated with Method Deviations	mg/m ³	0.29	0.28	0.86	
Reported Uncertainty	mg/m ³	0.29	0.28	0.86	
Expanded uncertainty (95% confidence), without Oxygen Correction	%	6.3	6.7	5.1	
Expanded uncertainty (95% confidence), with Oxygen Correction	%	N/A	N/A	N/A	
Expanded uncertainty (95% confidence), estimated with Method Deviations	%	6.3	6.7	5.1	
Reported Uncertainty	%	6.3	6.7	5.1	

HYDROGEN FLUORIDE(ISO): RESULTS SUMMARY

Furness Brick and Tile Company Ltd, Askam-in-Furness
Main Kiln Stack

Sample Runs

Parameter	Units	Run 1	Run 2	Run 3		Mean
Concentration	mg/m ³	0.24	0.48	2.3		1.0
Uncertainty	±mg/m ³	0.02	0.03	0.17		0.07
Mass Emission	g/hr	26.3	53.9	257		113
Uncertainty	±g/hr	3.0	6.2	29.8		13.0

Parameter	Units	Run 1	Run 2	Run 3		Mean
Water Vapour	% v/v	3.0	3.1	2.5		2.9
Uncertainty	±% v/v	0.15	0.16	0.13		0.14

NOTE: Where water droplets are present (See the Quality Assurance page), the Water Vapour concentration as found in Annex A of EN 14790 has been reported instead of the calculated value.

Blank Runs

Parameter	Units	Blank 1		Maximum
Concentration	mg/m ³	< 0.01		< 0.01

General Sampling Information

Parameter	Value
Standard	BS ISO 15713
Technical Procedure	CAT-TP-10
Name of Analytical Laboratory	CAT
Analytical Laboratory's Procedure	CAT-AP-01
ISO 17025 Accredited Analysis?	Yes
Date of Sample Analysis	30/12/2015
Probe Material	Monel
Filter Housing Material	Monel
Impinger Material	Polyethylene
Absorption Solution	0.1 mol/l Sodium Hydroxide
Positioning of Filter	In Stack
Filter Size and Material	47mm Quartz Fibre
Number of Sampling Lines Used	1 / 3
Number of Sampling Points Used	10 / 10
Sample Point I.D.'s	A1, A2, A3, A4, A5, A6, A7, A8, A9 & A10.

FORMAT: Number Used / Number Required

FORMAT: Number Used / Number Required

Reference Conditions

Reference Conditions are: 273K, 101.3kPa, without correction for water vapour content.

HYDROGEN FLUORIDE(ISO): ISOKINETIC SAMPLING CALCULATIONS

Test	Units	Run 1	Run 2	Run 3	
Absolute pressure of stack gas, P_s					
Barometric pressure, P_b	mmHg	744.8	744.8	744.8	
Stack static pressure, P_{static}	mmH ₂ O	7.9	7.9	7.9	
$P_s = (P_b + (P_{static} / 13.6))$	mmHg	745.3	745.3	745.3	
Volume of water vapour collected, V_{wstd}					
Total mass collected in impingers (liquid trap)	g	25.5	46.5	38.1	
Total mass collected in impingers (silica trap)	g	37.8	17.0	3.3	
Total mass of liquid collected, V_{lc}	g	63.3	63.5	41.4	
$V_{wstd} = (0.001246)(V_{lc})$	m ³	0.0789	0.0791	0.0516	
Volume of gas metered dry, V_{mstd}					
Volume of gas sample through gas meter, V_m	m ³	2.3479	2.2656	2.0479	
Gas meter correction factor, Y_d	-	1.0580	1.0580	1.0580	
Average dry gas meter temperature, T_m	°C	20.6	23.0	18.6	
Average pressure drop across orifice, ΔH	mmH ₂ O	19.7	18.6	15.7	
$V_{mstd} = ((0.3592)(V_m)(P_b + (\Delta H/13.6))(Y_d)) / (T_m + 273)$	m ³	2.2681	2.1703	1.9906	
Moisture content, B_{wo} & R_{ww}					
$B_{wo} = V_{wstd} / (V_{mstd} + V_{wstd})$	m ³	0.0336	0.0352	0.0253	
B_{wo} as a percentage	% v/v	3.36	3.52	2.53	
Reported Water Vapour, checked with Tables in EN 14790, R_{ww}	% v/v	2.96	3.14	2.53	
Volume of gas metered wet, V_{mstw}					
$V_{mstw} = (V_{mstd})(100/(100 - R_{ww}))$	m ³	2.3373	2.2407	2.0421	
Volume of gas metered at Oxygen Reference Conditions, $V_{mstd@X\%O_2}$ & $V_{mstw@X\%O_2}$					
IED & Incinerates Hazardous Material? (Yes = no positive O ₂ correction)	-	No	No	No	
% wet oxygen measured in gas stream, ACT%O _{2w}	% v/v	N/A	N/A	N/A	
% dry oxygen measured in gas stream, ACT%O _{2d}	% v/v	N/A	N/A	N/A	
% oxygen reference condition, REF%O ₂	% v/v	N/A	N/A	N/A	
O ₂ Reference Factor wet ($O_{2REFw} = (21 - REF\%O_2) / (21 - ACT\%O_{2w})$)	-	N/A	N/A	N/A	
O ₂ Reference Factor dry ($O_{2REFd} = (21 - REF\%O_2) / (21 - ACT\%O_{2d})$)	-	N/A	N/A	N/A	
$V_{mstw@X\%oxygen} = (V_{mstw}) / (O_{2REFw})$	m ³	N/A	N/A	N/A	
$V_{mstd@X\%oxygen} = (V_{mstd}) / (O_{2REFd})$	m ³	N/A	N/A	N/A	
Molecular weight of dry gas stream, M_d					
CO ₂ (Estimated)	% v/v	0.06	0.06	0.06	
O ₂ (Estimated)	% v/v	20.80	20.80	20.80	
Total	% v/v	20.86	20.86	20.86	
N ₂	% v/v	79.14	79.14	79.14	
$M_d = 0.44(\%CO_2) + 0.32(\%O_2) + 0.28(\%N_2)$	g/gmol	28.84	28.84	28.84	
Molecular weight of stack gas (wet), M_s					
$M_s = M_d(1 - (R_{ww}/100)) + 18(R_{ww}/100)$	g/gmol	28.52	28.50	28.57	
Velocity of stack gas, V_s					
Pitot tube velocity constant, K_p	-	34.97	34.97	34.97	
Velocity pressure coefficient, C_p	-	0.85	0.85	0.85	
Average of velocity heads, ΔP_{avg}	mmH ₂ O	5.30	4.88	4.23	
Average square root of velocity heads, $\sqrt{\Delta P}$	√mmH ₂ O	2.30	2.21	2.06	
Average stack gas temperature, T_s	°C	23.5	24.8	28.0	
$V_s = ((K_p)(C_p)(\sqrt{\Delta P})(T_s + 273)) / (V(M_s)(P_s))$	m/s	8.10	7.79	7.28	
Total flow of stack gas: Actual (Q_a), Wet (Q_{stw}), Dry (Q_{std}), Wet@O_{2REF} (Q_{stwO_2}), Dry@O_{2REF} (Q_{stdO_2})					
Area of stack, A_s	m ²	4.66	4.66	4.66	
$Q_a = (60)(A_s)(V_s)$	m ³ /min	2266.0	2180.5	2037.2	
Conversion factor (K/mm.Hg), C_f	-	0.3592	0.3592	0.3592	
$Q_{stw} = ((Q_a)(P_s)(C_f)) / ((T_s) + 273)$	m ³ /min	2045.9	1960.3	1811.9	
$Q_{std} = ((Q_a)(P_s)(C_f)(1 - (R_{ww}/100))) / ((T_s) + 273)$	m ³ /min	1985.3	1898.8	1766.1	
$Q_{stwO_2} = ((Q_a)(P_s)(C_f)) / ((T_s) + 273) / (O_{2REFw})$	m ³ /min	N/A	N/A	N/A	
$Q_{stdO_2} = ((Q_a)(P_s)(C_f)(1 - (R_{ww}/100))) / ((T_s) + 273) / (O_{2REFd})$	m ³ /min	N/A	N/A	N/A	
Percent isokinetic, %I					
Nozzle diameter, D_n	mm	6.05	6.05	6.05	
Nozzle area, A_n	mm ²	28.72	28.72	28.72	
Total sampling time, q	min	180	180	180	
$\%I = (4.6398E^6)(T_s + 273)(V_{mstd}) / (P_s)(V_s)(A_n)(q)(1 - (R_{ww}/100))$	%	103.0	103.1	101.7	

HYDROGEN FLUORIDE(ISO): SAMPLING DETAILS

Sample Runs

Parameter	Units	Run 1	Run 2	Run 3	
Sampling Times	-	11:40 - 14:40	14:50 - 17:50	09:22 - 12:22	
Sampling Dates	-	15/12/2015	15/12/2015	16/12/2015	
Sampling Device	-	ISO	ISO	ISO	
Volume Sampled (REF)	m ³	2.3373	2.2407	2.0421	
Laboratory Result for Front Impingers	µg/ml	1.06	2.12	9.12	
Laboratory Result for Back Impinger	µg/ml	0.05			
Volume in Front Impingers	ml	507.6	509.2	515.0	
Volume in Back Impinger	ml	232.7			
Mass in Front Impingers	µg	538.1	1079.5	4696.8	
Mass in Back Impinger	µg	< 11.6			
Total Mass Collected	µg	549.7	1079.5	4696.8	
Calculated Concentration	mg/m ³	0.24	0.48	2.30	

Where: ISO stands for Manual Isokinetic Sampling Train

Blank Runs

Parameter	Units	Blank 1	
Blank Dates	-	15/12/2015	
Average Volume Sampled (REF)	m ³	2.2067	
Laboratory Result for Impingers	µg/ml	< 0.05	
Volume in Impingers	ml	427.3	
Total Mass Collected	µg	< 21.4	
Calculated Concentration	mg/m ³	< 0.01	

HYDROGEN FLUORIDE(ISO): QUALITY ASSURANCE

(PAGE 1 OF 2)

Sample Runs

Leak Test Results	Units	Run 1	Run 2	Run 3	
Mean Sampling Rate	l/min	13.80	13.32	12.04	
Pre-Sampling Leak Rate	l/min	0.06	0.15	0.09	
Post-Sampling Leak Rate	l/min	0.14	0.11	0.14	
Allowable Leak Rate	l/min	0.28	0.27	0.24	
Leak Test Acceptable	-	Yes	Yes	Yes	

Absorption Efficiency	Units	Run 1	
Absorption Efficiency	%	100.0	
Allowable Absorption Efficiency	%	N/A	
Absorption Efficiency Acceptable	-	N/A	

The concentration is less than 30% of the ELV, therefore no assessment against an allowable efficiency is required.

Water Droplets	Units	Run 1	Run 2	Run 3	
Are Water Droplets Present	-	Yes	Yes	No	

MU (Concurrent Water Vapour)	Units	Run 1	Run 2	Run 3	
Measurement Uncertainty (MU)	%	5.0	5.0	5.1	
Allowable MU	%	20	20	20	
MU Acceptable	%	Yes	Yes	Yes	

Silica Gel (Concurrent Water Vapour)	Units	Run 1	Run 2	Run 3	
Less than 50% Faded	%	Yes	Yes	Yes	

Isokinetic Criterion Compliance	Units	Run 1	Run 2	Run 3	
Isokinetic Variation	%	103.0	103.1	101.7	
Allowable Isokinetic Range	%	95 - 115	95 - 115	95 - 115	
Isokineticity Acceptable	-	Yes	Yes	Yes	

Filter Temperatures	Units	Run 1	Run 2	Run 3	
Maximum Filter Temperature	°C	24	25	28	

Test Conditions	Units	Run 1	Run 2	Run 3	
Ambient Temperature Recorded?	-	Yes	Yes	Yes	

HYDROGEN FLUORIDE(ISO): QUALITY ASSURANCE

(PAGE 2 OF 2)

Blank Runs

Leak Test Results	Units	Blank 1	
Expected Sampling Rate	l/min	15.00	
Pre-Sampling Leak Rate	l/min	0.09	
Post-Sampling Leak Rate	l/min	0.13	
Allowable Leak Rate	l/min	0.30	
Leak Test Acceptable	-	Yes	

Validity of Blank vs ELV	Units	Blank 1	
Allowable Blank	mg/m ³	1.0	
Blank Acceptable	-	Yes	

Method Deviations

Nature of Deviation	Run Number			
	1	2	3	
(x = deviation applies to the associated run, wx = deviation also applies to the concurrent water vapour run)				
There are no deviations associated with the sampling employed.	wx	wx	wx	

HYDROGEN FLUORIDE(ISO): MEASUREMENT UNCERTAINTY CALCULATIONS

Measured Quantities	Value					Symbol	Standard uncertainty				
	Symbol	Run 1	Run 2	Run 3			Units	Run 1	Run 2	Run 3	
Sampled Volume (Actual)	V _m	2.3479	2.2656	2.0479		uV _m	m ³	0.0470	0.0453	0.0410	
Sampled Gas Temperature	T _m	293.6	296.0	291.6		uT _m	K	2.0	2.0	2.0	
Sampled Gas Pressure	p _m	99.4	99.4	99.4		up _m	kPa	0.5	0.5	0.5	
Sampled Gas Humidity	H _m	0.0	0.0	0.0		uH _m	% v/v	1.0	1.0	1.0	
Leak	L	1.01	0.83	1.16		uL	%	-	-	-	
Laboratory Result	L _r	2.65	2.65	2.65		uL _r	%	-	-	-	

Measured Quantities	Uncertainty as a Percentage					Requirement of Standard
	Units	Run 1	Run 2	Run 3		
Sampled Volume (Actual)	%	2.00	2.00	2.00		≤2%
Sampled Gas Temperature	%	0.68	0.68	0.69		≤1%
Sampled Gas Pressure	%	0.50	0.50	0.50		≤1%
Sampled Gas Humidity	%	1.00	1.00	1.00		≤1%
Leak	%	1.01	0.83	1.16		≤2%
Laboratory Result	%	2.65	2.65	2.65		No Requirement

Measured Quantities	Uncertainty in Measurement Units					Symbol	Sensitivity Coefficient			
	Units	Run 1	Run 2	Run 3			Run 1	Run 2	Run 3	
Sampled Volume (STP)	V _m	m ³	2.2681	2.1703	1.9906		0.10	0.22	1.16	
Leak	L	mg/m ³	0.0014	0.0023	0.0154		1.00	1.00	1.00	
Laboratory Result	L _r	mg/m ³	0.006	0.013	0.061		1.00	1.00	1.00	

Measured Quantities	Uncertainty in Result				
	Units	Run 1	Run 2	Run 3	
Sampled Volume (STP)	mg/m ³	0.0058	0.0119	0.0561	
Leak	mg/m ³	0.001	0.002	0.015	
Laboratory Result	mg/m ³	0.006	0.013	0.061	

Measured Quantities	Oxygen Correction Part of MU Budget				
	Units	Run 1	Run 2	Run 3	
O ₂ Correction Factor	-	N/A	N/A	N/A	
Stack Gas O ₂ Content	% v/v	N/A	N/A	N/A	
MU for O ₂ Correction	-	N/A	N/A	N/A	
Overall MU For O ₂ Measurement	%	N/A	N/A	N/A	

Parameter	Units	Run 1	Run 2	Run 3	
Combined uncertainty	mg/m ³	0.01	0.02	0.08	
Expanded uncertainty (95% confidence), without Oxygen Correction	mg/m ³	0.02	0.03	0.17	
Expanded uncertainty (95% confidence), with Oxygen Correction	mg/m ³	N/A	N/A	N/A	
Expanded uncertainty (95% confidence), estimated with Method Deviations	mg/m ³	0.02	0.03	0.17	
Reported Uncertainty	mg/m ³	0.02	0.03	0.17	
Expanded uncertainty (95% confidence), without Oxygen Correction	%	7.2	7.2	7.2	
Expanded uncertainty (95% confidence), with Oxygen Correction	%	N/A	N/A	N/A	
Expanded uncertainty (95% confidence), estimated with Method Deviations	%	7.2	7.2	7.2	
Reported Uncertainty	%	7.2	7.2	7.2	

HYDROGEN FLUORIDE (NON ISO): RESULTS SUMMARY

Furness Brick and Tile Company Ltd, Askam-in-Furness
Main Kiln Stack

Sample Runs

Parameter	Units	Run 1	Run 2		Mean
Concentration	mg/m ³	0.69	1.3		1.0
Uncertainty	±mg/m ³	0.05	0.09		0.07
Mass Emission	g/hr	77.6	150		114
Uncertainty	±g/hr	8.7	16.8		12.7

Parameter	Units	Run 1	Run 2		Mean
Water Vapour	% v/v	2.7	2.9		2.8
Uncertainty	±% v/v	0.11	0.12		0.11

General Sampling Information

Parameter	Value
Standard	ISO 15713
Technical Procedure	CAT-TP-10
Name of Analytical Laboratory	CAT
Analytical Laboratory's Procedure	CAT-AP-01
ISO 17025 Accredited Analysis?	Yes
Date of Sample Analysis	30/12/2015
Probe Material	Monel
Filter Housing Material	Monel
Impinger Material	Polyethylene
Absorption Solution	0.1 mol/l Sodium Hydroxide
Positioning of Filter	Out Stack
Filter Size and Material	47mm Quartz Fibre
Number of Sampling Lines Used	1 / 1
Number of Sampling Points Used	1 / 1
Sample Point I.D.'s	A6

FORMAT: Number Used / Number Required

FORMAT: Number Used / Number Required

Reference Conditions

Reference Conditions are: 273K, 101.3kPa, without correction for water vapour content.

HYDROGEN FLUORIDE (NON ISO): SAMPLING DETAILS

Sample Runs

Parameter	Units	Run 1	Run 2	
Sampling Times	-	18:00 - 00:00	00:10 - 09:10	
Sampling Dates	-	15/12/2015	16/12/2015	
Sampling Device	-	MFC / MV	MFC / MV	
Duration	mins	360	540	
Volume Sampled (STP, Dry)	m ³	3.6455	3.9534	
Volume Sampled (STP, Wet)	m ³	3.7476	4.0696	
Volume Sampled (REF)	m ³	3.7476	4.0696	
Sample Flow Rate	l/min	10.12	7.32	
Laboratory Result for Front Impingers	µg/ml	4.57	9.64	
Laboratory Result for Back Impinger	µg/ml	0.05		
Volume in Front Impingers	ml	567.3	565.7	
Volume in Back Impinger	ml	149.3		
Mass in Front Impingers	µg	2592.6	5453.3	
Mass in Back Impinger	µg	< 7.5		
Total Mass Collected	µg	2600.0	5453.3	
Calculated Concentration	mg/m ³	0.69	1.34	
Liquid Trap Start Mass	g	1814.0	1829.6	
Liquid Trap End Mass	g	1877.2	1915.0	
Silica Trap Start Mass	g	1035.7	1039.6	
Silica Trap End Mass	g	1054.5	1047.5	
Total Mass Of Water Vapour	g	82.0	93.3	
Calculated Water Vapour	% v/v	2.73	2.86	

Where: MFC stands for Mass Flow Controller, MV stands for Mass View Flowmeter

HYDROGEN FLUORIDE (NON ISO): QUALITY ASSURANCE

Sample Runs

Leak Test Results	Units	Run 1	Run 2	
Mean Sampling Rate	l/min	10.12	7.32	
Pre-Sampling Leak Rate	l/min	0.05	0.05	
Post-Sampling Leak Rate	l/min	0.00	0.04	
Allowable Leak Rate	l/min	0.20	0.15	
Leak Test Acceptable	-	Yes	Yes	

Absorption Efficiency	Units	Run 1	
Absorption Efficiency	%	100.0	
Allowable Absorption Efficiency	%	N/A ²	
Absorption Efficiency Acceptable	-	N/A ²	

² The concentration is less than 30% of the ELV, therefore no assessment against an allowable efficiency is required.

Water Droplets	Units	Run 1	Run 2	
Are Water Droplets Present	-	No	No	

MU (Concurrent Water Vapour)	Units	Run 1	Run 2	
Measurement Uncertainty (MU)	%	4.0	4.1	
Allowable MU	%	20	20	
MU Acceptable	%	Yes	Yes	

Silica Gel (Concurrent Water Vapour)	Units	Run 1	Run 2	
Less than 50% Faded	%	Yes	Yes	

Test Conditions	Units	Run 1	Run 2	
Ambient Temperature Recorded?	-	Yes	Yes	

Method Deviations

Nature of Deviation	Run Number	
	1	2
(x = deviation applies to the associated run, wx = deviation also applies to the concurrent water vapour run)		
There are no deviations associated with the sampling employed.	wx	wx

HYDROGEN FLUORIDE (NON ISO): MEASUREMENT UNCERTAINTY CALCULATIONS

Measured Quantities	Value				Symbol	Standard uncertainty			
	Symbol	Run 1	Run 2			Units	Run 1	Run 2	
Sampled Volume (STP)	V _m	3.6455	3.9534		uV _m	m ³	0.0729	0.0791	
Leak	L	0.00	0.55		uL	%	-	-	
Laboratory Result	L _r	2.65	2.65		uL _r	%	-	-	

Measured Quantities	Uncertainty as a Percentage				Requirement of Standard
	Units	Run 1	Run 2		
Sampled Volume (STP)	%	2.00	2.00		≤2%
Leak	%	0.00	0.55		≤2%
Laboratory Result	%	2.65	2.65		No Requirement

Measured Quantities	Uncertainty in Measurement Units					Sensitivity Coefficient		
	Symbol	Units	Run 1	Run 2		Run 1	Run 2	
Sampled Volume (STP)	V _m	m ³	3.6455	3.9534		0.19	0.34	
Leak	L	mg/m ³	0.000	0.004		1.00	1.00	
Laboratory Result	L _r	mg/m ³	0.018	0.036		1.00	1.00	

Measured Quantities	Uncertainty in Result			
	Units	Run 1	Run 2	
Sampled Volume (STP)	mg/m ³	0.0139	0.0268	
Leak	mg/m ³	0.0000	0.0042	
Laboratory Result	mg/m ³	0.0184	0.0355	

Measured Quantities	Oxygen Correction Part of MU Budget			
	Units	Run 1	Run 2	
O ₂ Correction Factor	-	N/A	N/A	
Stack Gas O ₂ Content	% v/v	N/A	N/A	
MU for O ₂ Correction	-	N/A	N/A	
Overall MU For O ₂ Measurement	%	N/A	N/A	

Parameter	Units	Run 1	Run 2	
Combined uncertainty	mg/m ³	0.02	0.04	
Expanded uncertainty (95% confidence), without Oxygen Correction	mg/m ³	0.05	0.09	
Expanded uncertainty (95% confidence), with Oxygen Correction	mg/m ³	N/A	N/A	
Expanded uncertainty (95% confidence), estimated with Method Deviations	mg/m ³	0.05	0.09	
Reported Uncertainty	mg/m ³	0.05	0.09	
Expanded uncertainty (95% confidence), without Oxygen Correction	%	6.5	6.5	
Expanded uncertainty (95% confidence), with Oxygen Correction	%	N/A	N/A	
Expanded uncertainty (95% confidence), estimated with Method Deviations	%	6.5	6.5	
Reported Uncertainty	%	6.5	6.5	